

## Extraction of Molybdenum (VI) With 4-Adipoyl and 4-Sebacoyl Derivatives of Bis (1-Phenyl-3-Methylpyrazolone-5) In Acid Media

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**Abstract:** Liquid – liquid extraction of Molybdenum (VI) ions from various aqueous medium have been carried out using chloroform solution of 4-adipoylbis (1-phenyl-3-methylpyrazolone-5), H<sub>2</sub>Adp and 4-sebacoylbis (1-phenyl-3-methylpyrazolone-5), H<sub>2</sub>SP in acid media (HCl, H<sub>2</sub>SO<sub>4</sub> and HNO<sub>3</sub>) in the presence and absence of butanol as a synergist. The degree of extraction of Mo (VI) using H<sub>2</sub>Adp was found to be in the range of 82 – 95% for HCl concentrations of 10<sup>-3</sup>M to 10<sup>-1</sup>M and 90 – 97% for HNO<sub>3</sub> (10<sup>-3</sup>M to 10<sup>-1</sup>M) while H<sub>2</sub>SO<sub>4</sub> concentrations gave 70% extraction. On the other hand, the degree of extraction of Mo(VI) using H<sub>2</sub>SP was comparatively lower in all acid media. Under all acid conditions studied, H<sub>2</sub>Adp was found to be a better extractant for Mo(VI) than H<sub>2</sub>SP, while optimal extraction was better in HCl followed by HNO<sub>3</sub> and least in H<sub>2</sub>SO<sub>4</sub> concentrations. However, introduction of butanol into the organic phase resulted in enhanced extraction of Mo(VI) to above 98% using both ligands in all three acid media for both H<sub>2</sub>Adp and H<sub>2</sub>SP. Statistical treatment using slope analysis show that the extracted specie is MoO<sub>2</sub>(SP)<sub>(o)</sub> and MoO<sub>2</sub>(Adp)<sub>(o)</sub>.

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**Keywords:** Liquid – liquid extraction, chloroform, Molybdenum (VI), acid media

### 1. Introduction

Extraction of metals using various ligands has been an on going study over the years. Hence the search for more ligands and better conditions for extraction of various metals cannot be over emphasized. In view of this, the ligands 4-adipoylbis (1-phenyl-3-methylpyrazolone-5), (H<sub>2</sub>Adp) and 4-sebacoylbis (1-phenyl-3-methylpyrazolone-5), (H<sub>2</sub>SP) which were first synthesized and characterized by Okafor and Uzoukwu (1991) having been found to exhibit the ability of effectively trapping toxic metals such as Fe, Cd, Cu, Ni, Mn, U, V and W from water, was considered for this study. Their extensive use in organic solutions as extractants (Bukowsky et al (1992), Uzoukwu and Okafor 1990, Uzoukwu et al 1996, 1998) has been demonstrated. They are β diketones, and like other 4-acylpyrazolones have equally proven to be efficient metal extractants forming stable complexes with some group I, II and many transition metals (Okafor, et al, 1993; Uzoukwu and Adiukwu, 1996; Chukwu and Uzoukwu, 2010). Introduction of various synergists have further improved the efficiency of these ligands in solvent extraction studies (Umetani et al 1990; Atanassova and Dukov, 2006; Bond et al, 1999).

Therefore, this present work, aims at extraction of Molybdenum (VI) from concentrations of different acid media (HCl, HNO<sub>3</sub> and H<sub>2</sub>SO<sub>4</sub>) using 4-adipoylbis (1-phenyl-3-methylpyrazolone-5), H<sub>2</sub>Adp and 4-sebacoylbis (1-phenyl-3-methylpyrazolone-5) H<sub>2</sub>SP in chloroform. The distribution behavior of the metal ions in the organic phase containing these chelating agents in the presence and absence of butanol will also be studied.

### 2. Experimental

#### 2.1 Materials

All reagents used were of analytical grade (Merck or BDH). They include HCl, HNO<sub>3</sub>, H<sub>2</sub>SO<sub>4</sub>, Butanol, ammonium molybdate hydrate, Chloroform (CHCl<sub>3</sub>). Deionized water was used throughout the experiment. Consort C531 pH/conductivity meter, BioBlock UV Spectrophotometer, Mechanical Shaker and extraction bottles were used.

#### 2.2 Analytical Methods

Stock solutions of 0.01M of H<sub>2</sub>Adp and H<sub>2</sub>SP were prepared by dissolving the appropriate mass of the ligand (H<sub>2</sub>Adp and H<sub>2</sub>SP) each in Chloroform (CHCl<sub>3</sub>). These solutions (H<sub>2</sub>Adp and H<sub>2</sub>SP) were stable for at least one

month. Stock solution (100mgL<sup>-1</sup>) of the metal ion Mo(VI) was equally prepared by dissolving appropriate mass of ammonium molybdate hydrate.

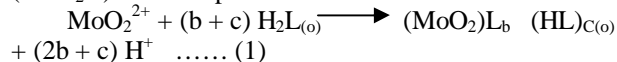
The aqueous phase was made up of 0.1ml aliquot of the metal ion stock solution followed by a solution of acid and deionized water to give 1ml such that the final dilution gave different concentrations of 0.001M to 5M for the acid. An equal volume (1ml) of 0.01M solution of H<sub>2</sub>Adp / CHCl<sub>3</sub> and H<sub>2</sub>SP / CHCl<sub>3</sub> was added respectively to make up the organic phase. This mixture was shaken mechanically for 30 minutes at room temperature. A shaking time of 30 minutes was found to be enough for equilibration. The phases were allowed to settle and then separated for analysis of the metal ion in the aqueous raffinate. Extraction in the presence of synergist was prepared using the same procedure. However, the organic phase was prepared using the extractants (H<sub>2</sub>Adp and H<sub>2</sub>SP) in a CHCl<sub>3</sub>/BuOH mixture in the ratio 4:1.

The Mo(VI) ions in the aqueous raffinate were determined using established techniques (Jeffrey et al, 1987, Allen et al, 1974). A 0.5ml volume of the Mo(VI) extraction raffinate was introduced into 5ml sample bottle. Subsequently, 1ml of 60% HCl was added to acidify the solution, followed by 0.5ml of 20% NH<sub>4</sub>SCN. A 0.2ml volume of freshly prepared 5% Ascorbic acid was added to form a cherry red complex. The solution mixture was made up to 5ml with deionized water. The absorbance of the cherry red complex was read at 470nm against a blank using a BioBlock UV Spectrophotometer. The amount of Mo(VI) in the aqueous solution after extraction was determined by comparing the absorbance of the solution with that of a standard calibration curve. The concentration of metal ion extracted into the organic phase was determined by difference. Distribution ratio, D, was calculated as the ratio of metal ion concentration in organic phase (C<sub>o</sub>) to that in the aqueous phase (C) thus,  $D = C_o/C$ .

### 3. Results and discussion

#### 3.1 Theoretical considerations

Earlier works of Uzoukwu et al (1998<sup>a</sup>) have shown that these ligands are weak organic acids and therefore behaved as 4-acylbispyrazolone chelating acids in solution. Thus the extraction of the metals species (MoO<sub>2</sub><sup>2+</sup>) can be represented as follows.



Where H<sub>2</sub>L is the 4-acylbispyrazolone

$$K_{\text{ex1}} = \frac{[(\text{MoO}_2)_\text{L}_b (\text{HL})_\text{C}_{(o)}] [\text{H}^+]^{(2b+c)}}{[\text{MoO}_2^{2+}] [\text{H}_2\text{L}]_{(o)}^{(b+c)}} \dots\dots (2)$$

Where K<sub>ex1</sub> is the extraction constant. Hence the distribution ratio D is given by:

$$\log D_1 = \log K_{\text{ex1}} + (b + c) \log [\text{H}_2\text{L}]_o - (2b + c) \log [\text{H}^+] \dots\dots (3)$$

In the presence of a solvating agent such as butanol (BuOH), the distribution ration becomes:

$$\log D_2 = \log K_{\text{ex2}} + (b + c) \log [\text{H}_2\text{L}]_{(o)} + d \log [\text{BuOH}]_{(o)} - (2b + c) \log [\text{H}^+] \dots\dots (4)$$

where (MoO<sub>2</sub>)L<sub>b</sub>(HL)<sub>c</sub>(<sub>o</sub>) and (MoO<sub>2</sub>)L<sub>b</sub>(HL)<sub>c</sub>(BuOH)<sub>d</sub>(<sub>o</sub>) represent the extractable metal complexes in the absence and presence of butanol respectively

Determination of the values of b, c, and d for interactions between the ligand and one mole of metal in the equations can be done through evaluation of the partial derivatives of the equations by the method of slope analysis as follows:

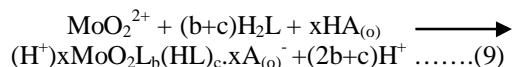
$$\frac{d[\log D]}{d[\log [\text{H}^+]]} = (2b + c) \dots\dots (5)$$

$$\frac{d[\log D]}{d[\log [\text{H}_2\text{L}]_o]} = b + c \dots\dots (6)$$

$$\frac{d[\log D]}{d[\log [\text{BuOH}]_{(o)}]} = d \dots\dots (7)$$

$$\frac{d[\log D]}{d[\log [\text{H}^+]]} = (a - 1) \dots\dots (8)$$

If an acid is involved as a solvating agent in the extraction of the metal, the expected ion pair complex that would be extracted can be described by the following equation as proposed by Okafor and Uzoukwu (1990).



$$K_{\text{ex3}} = \frac{[(\text{H}^+)_x\text{MoO}_2\text{L}_b(\text{HL})_c.x\text{A}^-]_{(o)} (\text{H}^+)^{2b+c}}{[\text{MoO}_2^{2+}] [\text{H}_2\text{L}]_{(o)}^{b+c} [\text{HA}]^x} \dots\dots (10)$$

$$D_3 = \frac{[(\text{H}^+)_x\text{MoO}_2\text{L}_b(\text{HL})_c.x\text{A}^-]_{(o)}}{[\text{MoO}_2^{2+}]} \dots\dots (11)$$

$$\log D_3 = \log K_{\text{ex3}} + (a-1) \log [\text{M}^{2+}] + (b+c) \log [\text{H}_2\text{L}]_{(o)} + e \log [\text{HA}] + (2b+c) \log \text{H}^+ \dots\dots (12)$$

Determination of the value of e in the equations can be done through evaluation of the partial derivative of the equation by the method of slope analysis as follows:

$$\frac{d[\log D_3]}{d[\log [\text{HA}]]} = e \dots\dots (13)$$

Evaluation of the quantities b, c, d and e will enable the stoichiometry of the extraction process for each of the extraction systems to be elucidated.

### 3.2 Extraction of Mo(VI) in the presence and absence of BuOH

Presented in Fig. 1 are plots of % extraction of Mo(VI) against acid concentrations of HCl, H<sub>2</sub>SO<sub>4</sub> and HNO<sub>3</sub> for extraction using H<sub>2</sub>Adp in the presence and absence of BuOH as a synergist. The result shows generally, that below 0.1M acid concentrations close to 98% extraction was achieved by the ligand, both in the presence and absence of BuOH as a solvating agent. However, in the extraction of the metal from H<sub>2</sub>SO<sub>4</sub> acid concentrations, a maximum of 70% extraction was achieved at 0.001M H<sub>2</sub>SO<sub>4</sub> acid concentration and this falls monotonously to less than 1% extraction at 0.5M H<sub>2</sub>SO<sub>4</sub> acid concentration. This trend is similar to what was reported by Koladkar and Dhadke (2002) on the solvent extraction of Sc (III) from H<sub>2</sub>SO<sub>4</sub> acid with PIA – 8 in toluene. The distribution ratio of Sc (III) decreased with increasing H<sub>2</sub>SO<sub>4</sub> acid concentration while quantitative extraction was obtained at H<sub>2</sub>SO<sub>4</sub> concentration range of 0.1 – 0.5M.

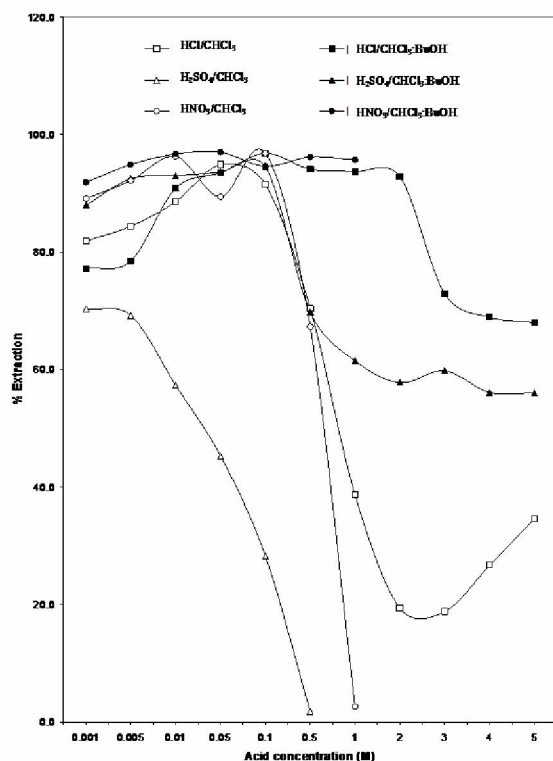


Figure 1: Variation of % Extraction of Mo(VI) with acid concentration for H<sub>2</sub>Adp.

The synergist effect of BuOH was very obvious in the extraction of Mo(VI) from various H<sub>2</sub>SO<sub>4</sub> concentrations as shown in Fig. 1, with almost 96% extraction of Mo(VI) at 0.01M H<sub>2</sub>SO<sub>4</sub> acid concentration. This also fell monotonously but not drastically as was the case in the absence of BuOH in the organic phase. Hence 58 – 68% extraction was achieved even at high acid concentrations of 1M – 5M H<sub>2</sub>SO<sub>4</sub>.

Extraction from HCl and HNO<sub>3</sub> solutions also showed evidence of the synergistic effect of BuOH in the organic phase. Hence, between 96 – 98% was achieved for extractions using HCl when BuOH was introduced into the organic phase for all concentrations of HCl. However, in the absence of BuOH, this fell drastically to 0.5% at 1M HCl concentration.

For extractions using H<sub>2</sub>SP in the presence and absence of BuOH as a synergist, plots of % extraction of Mo(VI) against acid concentrations of HCl, H<sub>2</sub>SO<sub>4</sub> and HNO<sub>3</sub> is shown in Fig. 2.

Maximum % extraction was recorded at 80% and 50% for HCl and HNO<sub>3</sub> respectively between acid concentrations of 0.01M and 0.1M while at 0.001M H<sub>2</sub>SO<sub>4</sub> concentration maximum % extraction of 38% was achieved, but fell monotonously to 5% at 0.5M acid concentration. Introduction of butanol into the extraction process enhanced the extraction of the metal ion in all the acid media with maximum % extraction of above 90% occurring between 0.5M and 0.05M acid concentrations for all three acids.

The results generally show that the synergist effect is more pronounced for extractions from H<sub>2</sub>SO<sub>4</sub> solution more than from HCl and HNO<sub>3</sub> solution and so the trend can be summarized as follows:

H<sub>2</sub>SO<sub>4</sub> > HCl ≈ HNO<sub>3</sub>  
 Decrease in BuOH synergism for Mo(VI) extraction

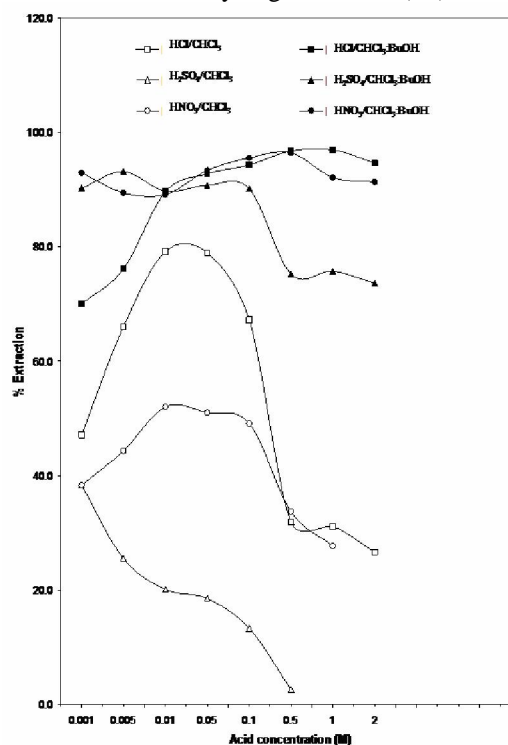


Figure 2: Variation of % Extraction of Mo(VI) with acid concentration for H<sub>2</sub>SP

From Figs. 1 and 2 above, the extraction of Mo(VI)

from various acid concentrations for both ligands show that optimal % extraction is minimal at H<sub>2</sub>SO<sub>4</sub> concentrations followed by HNO<sub>3</sub> and highest at HCl. This has been attributed to low [H<sup>+</sup>] concentration from the relatively weaker acid, in which case the strong anionic conjugate base from the weak acids tend to be more reactive with the metal ions and masking them at these low acid concentrations.

These results therefore suggest that H<sub>2</sub>Adp is a better extractant of the metal ion Mo(VI) than H<sub>2</sub>SP. This is probably due to the differences in the chain length and orientation of the carbon atoms in these chelating agents.

### 3.3 Extraction Mechanism of Mo(VI)

Statistical treatment of data using slope analysis as applied to this work has earlier been discussed as reported by Uzoukwu 1998; Uzoukwu et al 1998<sup>b</sup> and the mechanism of interaction presented in Figs 3 to 5. The mechanism of interaction between Mo(VI) and the ligands for H<sub>2</sub>SO<sub>4</sub>, HCl and HNO<sub>3</sub> solutions are presented as plots of log D versus log [Acid] in Fig 3.

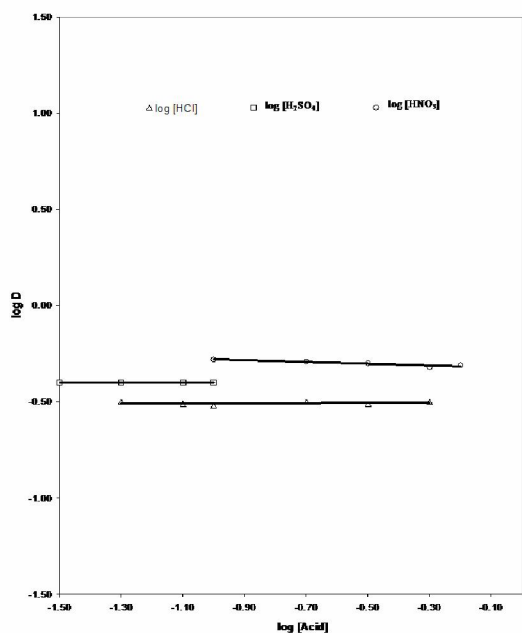


Figure 3: Plot of log D Vs log [Acid] for Mo(VI) with H<sub>2</sub>Adp

The plots on Figs 3 show that the slopes are zero; hence applying equation (12), the value of “x” is equal to zero. Equation (8) presented a situation in which the extraction of the metal may take place through ion pair complex formation. However, from the result obtained from the slope analysis, it is therefore evidenced experimentally that the acids were not incorporated in the complex during the extraction process. Therefore no ion pair complex was extracted into the organic phase. This shows that the appropriate equation for the extraction of

the non-ion pair complex is that of equation (1).

Figure 4 also shows that the slope obtained from plots of log D versus metal ion concentration is equal to zero as well. Hence, on applying statistical methods the extraction of the non-ion pair complex species implies that 1 mole of M<sub>0</sub>O<sub>2</sub><sup>2+</sup> is involved according to equation 8 where “a - 1=0”. This is an indication that 1 mole of the metal ion is involved in the extraction process since the log D plot is independent of changes in the metal ion concentration.

The interaction between the concentrations of the ligand is shown in figure 5 for the extraction of Mo(VI). A slope of one was recorded for all the three acids studied. Since there is no adduct complex formation as shown by the involvement of only 1 mole of Mo(VI) therefore “c” in equation (1) is then equal to zero. Hence from equation (6)

$$\begin{aligned} b + c &= 1 \\ b = 1 &\quad \text{since } c = 0 \end{aligned}$$

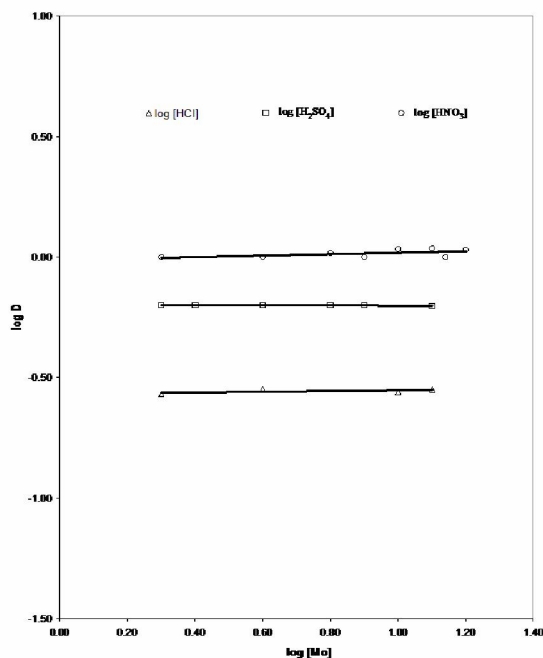
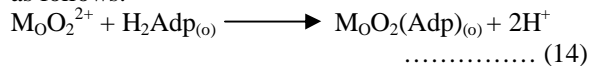


Figure 4: Plot of log D Vs log [Mo] with H<sub>2</sub>Adp.

With b = 1 and c = 0 this is an indication that 1 mole of the ligand was involved in the extraction process. Since it is a quadridentate ligand this implies that 2 moles of protons were released in the process.

Therefore the extraction process can be presented as follows:

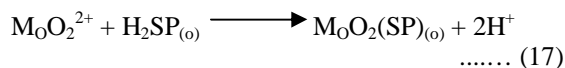


$$K_{ex} = \frac{[M_oO_2(Adp)_{(o)}][H^+]}{[M_oO_2^{2+}][H_2Adp]_{(o)}} \dots\dots\dots (15)$$

$$\log D = \log K_{ex} + \log [H_2Adp]_{(o)} - 2 \log [H^+] \dots\dots\dots (16)$$

Similarly, extraction of Mo(VI) using the ligand H<sub>2</sub>SP followed the same trend (fig 6).

Therefore the extraction process can equally be presented as follows:



$$K_{ex} = \frac{[M_oO_2(SP)_{(o)}][H^+]}{[M_oO_2^{2+}][H_2SP]_{(o)}} \dots\dots\dots (18)$$

$$\log D = \log K_{ex} + \log [H_2SP]_{(o)} - 2 \log [H^+] \dots\dots\dots (19)$$

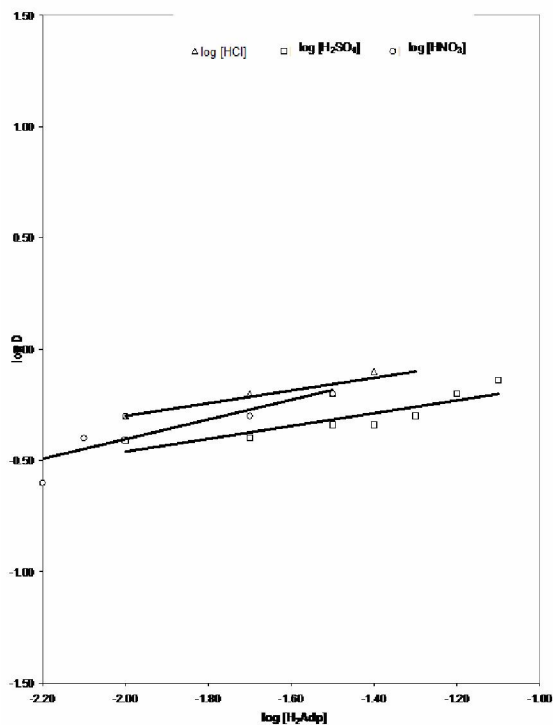


Figure 5: Plot of log D Vs log [H<sub>2</sub>Adp] with Mo(VI)

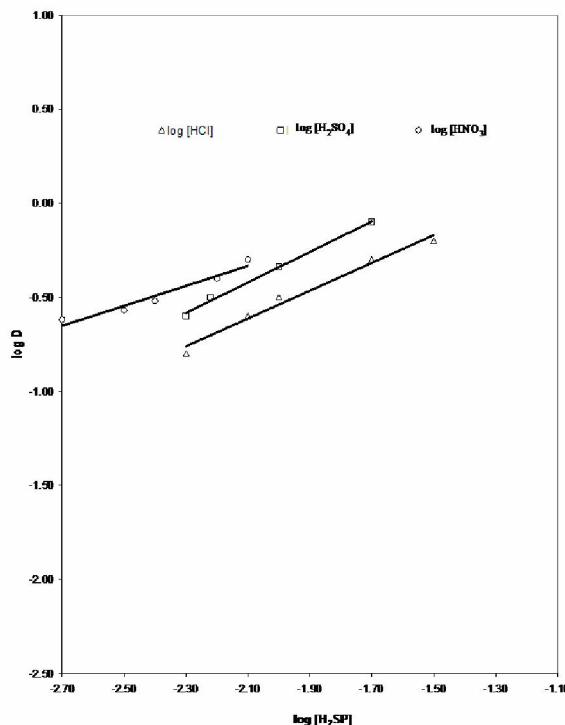


Figure 6: Plot of log D Vs log [H<sub>2</sub>SP] with Mo(VI)

#### 4. Conclusion

Extraction of Mo(VI) ions using 0.01M of the ligand H<sub>2</sub>Adp in chloroform from various acidic medium gave optimal % extraction above 90% within 0.01M and 0.5M acid concentrations for HCl and HNO<sub>3</sub> while extractions in H<sub>2</sub>SO<sub>4</sub> solutions gave a slightly lower % extraction yield of 70% within the concentration range of 0.001 and 0.005. In the case of the ligand H<sub>2</sub>SP, a much lower % extraction yield of 80% for HCl, 50% for HNO<sub>3</sub> and 39% for H<sub>2</sub>SO<sub>4</sub> was obtained within the same acid concentrations.

Introduction of butanol as a synergist into the extraction system greatly enhanced the overall optimal % extraction to 98% and 95% for extractions using 0.01M H<sub>2</sub>Adp and H<sub>2</sub>SP in chloroform respectively, within the acid concentrations of 0.01M and 1.0M in all cases. In addition, increase in acid concentrations above 1.0M has a masking effect on the extraction of Mo(VI) ions likewise very dilute acid concentration below 0.01M. Hence extraction of Mo(VI) using 0.01M H<sub>2</sub>Adp and H<sub>2</sub>SP in chloroform is best favored within the acid concentration of 0.01M and 1.0M.

Using theoretical considerations and slope analysis, the extracted species were found to be M<sub>o</sub>O<sub>2</sub>(Adp)<sub>(o)</sub> and M<sub>o</sub>O<sub>2</sub>(SP)<sub>(o)</sub>.

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