Extraction of Chromium (Vi) with 4-Adipoyl and 4-Sebacoyl Derivatives of Bis (1-Phenyl-3-Methylpyrazolone-5) in Acid Medium and the Effect of Butanol

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Abstract: Solvent extraction of chromium (VI) ions from concentrations of various mineral acids (HCl, H₂SO₄ and HNO₃) have been carried out using chloroform solution of 4-adipoylbis(1-phenyl-3-methylpyrazolone-5), H₂Adp and 4-sebacoylbis(1-phenyl-3-methylpyrazolone-5), H₂SP in the presence and absence of butanol (BuOH) as synergist. Cr(VI) was quantitatively extracted from all three mineral acids using 0.01M solutions of H₂Adp/chloroform and H₂SP/chloroform. Optimal % extraction of 62%, at 0.5M acid concentration was obtained for HCl and 66% at 1.0M for H₂SO₄. While 82% at 3.0M acid concentration was obtained for HNO₃ from chloroform solution of H₂Adp in the absence of BuOH. Similarly, H₂SP/chloroform solution gave optimal % extraction of 50%, 70% and 90% at 0.5M, 2.0M and 5.0M acid concentrations for HCl, H₂SO₄ and HNO₃ respectively, for the extraction of Cr(VI) in the absence of BuOH. In the presence of BuOH, synergism was more pronounced for extraction of Cr (VI) from HNO₃ and HCl solutions into organic solutions of H₂Adp and H₂SP respectively. However, optimum extraction was better in HNO₃ followed by H₂SO₄ and least in HCl acidic medium for extraction of Cr(VI) into organic solutions of 0.01M H₂Adp/chloroform and 0.01M H₂SP/chloroform in both the absence and presence of BuOH. Mechanism of the extraction systems showed that extraction using the ligand H₂SP first involves an acidification process followed by the extraction species as ion pair complexes. Hence, the extracted species were: $CrO_2(Adp)$ and $H_4CrO_4^{2+}(SP)^{2-}$ with an average log K_{ex} of 4.70.

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1.0 Introduction

1-phenyl-3-methyl-4-acylpyrazolone-5 and some of its derivatives have been widely reported in the extraction studies of many transition metals from different organic medium [1-5]. However, not so much has been reported on the bis derivative of this ligand [6-8]. The 4-adipoylbis(1-phenyl-3-methylpyrazolone-5), (H_2Adp) and 4-sebacoylbis(1-phenyl-3methylpyrazolone-5), (H₂SP) were synthesized for the first time and characterized by Okafor and Uzoukwu, [9]. They have been found to exhibit the ability of effectively trapping toxic metals such as Fe, Cd, Cu, Ni, Mn, U, V and W from water. This is the main reason for their proposed use in organic solutions as extractants [10-13]. Like the 4-acylpyrazolones, they are β diketones and are efficient extractants forming stable complexes with some group I, II and transition metals [9].

The object of this present work is to study the extraction of chromium (VI) with 4-adipoyl and 4-sebacoyl derivatives of bis(1-phenyl-3-methylpyrazolone-5), (H₂Adp and H₂SP) in three different acid medium (HCl, H₂SO₄ and HNO₃). In a related study, kalagbor et al [14] reported the extraction

of molybdenum (VI) with 4-adipoyl and 4-sebacoyl derivatives of bis(1-phenyl-3-methylpyrazolone-5) in acid medium. Furthermore, synergism has been demonstrated by several authors [15-18] in the extraction studies of 4-acylpyrazolone-5 to improve the efficiency of the ligand. Hence the present work equally aims at demonstrating synergism between these bisligand derivatives and butanol in the extraction of Chromium (VI) from concentrations of various mineral acids into chloroform solutions of 4-adipoylbis(1-phenyl-3-methylpyrazolone-5), and 4-sebacoylbis(1-phenyl-3-methylpyrazolone-5).

2.0 Experimental

2.1 Preparation of Stock Solutions

Fresh solutions of the organic extraction reagents, 4-adipoylbis(1-phenyl-3-methylpyrazolones-5) H_2Adp and 4-sebacoyl(1-phenyl-3methylpyrazolones-5) H_2SP were prepared as when required. Appropriate weights of the ligands (H_2Adp and H_2SP) were dissolved in CHCl₃ to give a 0.01M concentration of the working organic reagent. These solutions (H_2Adp and H_2SP) were stable for at least one month. Stock solution (100 mg/L) of the metal ion Cr(VI) was prepared in 0.001M HCl solution by dissolving appropriate weights of potassium chromate.

2.2 Extraction procedures

A 0.1cm^3 sample of the 100mg/L solution of Cr (VI) was pipetted into various sets of extraction bottles. A solution of an acid was added to each of the extraction bottles containing the metal ion followed by the addition of deionized water to adjust the volume of the aqueous solution in the bottles to 1 cm^3 such that the final dilution gave a range of concentrations from 0.001M to 5M of the acid.

An equal volume (1cm^3) of 0.01M solution of $H_2Adp/CHCl_3$ was added to each of the extraction bottles as the organic phase. The two phases were mechanically shaken for 30 minutes (which had previously been determined as the equilibration time) and allowed to separate, and the unextracted metal ions in the aqueous phase (aqueous raffinate) determined. Extractions with solutions of H_2SP / CHCl₃ were also carried out using the above method.

2.3 Extraction in the presence of a Synergist

Butanol was added as the synergist. The extractants (H_2Adp and H_2SP) were prepared using a CHCl₃ / BuOH mixture in the ratio of 4: 1. The resultant solution was a 0.01M standard solution of the extractants. The standard solutions were used for all levels of investigation.

2.4 Determination of the Metal Ion

The Cr (VI) ions present in the aqueous raffinate were determined using diphenylcarbazide (DPC) [19-20]. A 0.5cm^3 volume of the Cr (VI) extraction raffinate was taken and introduced into 5cm^3 sample bottles. A 0.5cm^3 volume of 10M H₂SO₄ was added followed by 1cm^3 of DPC forming a violet complex. The solution mixture was made up to 5cm^3 with deionized water. The absorbance of the complex was read at 540nm and the amount of Cr (VI) in the aqueous solution after extraction was determined by comparing the absorbance of the solution with that of a standard calibration curve.

The amount of metal extracted into the organic phase was obtained as the difference between the initial amount of metal ion concentration in the aqueous phase before extraction and the amount left in the aqueous phase after the extraction process, and is expressed as:

$$= \underbrace{[ML_n]_{(org)}}_{[M^{n+}]_{(aq)}}$$

where $[ML_n]_{org}$ is the metal chelate concentration in the organic phase.

 $[M^{n^{+}}]_{aq}$ is the metal ion concentration in the aqueous phase

3.0 Results and Discussion

D

3.1 Extraction of the Metal Species

Kalagbor et al [14] in a similar study with Mo(VI) ions had established the relationship between the metal ions and ligands in line with earlier works by Uzoukwu [21-22]. Thus the extraction of the metals species (M^{2+}) can be represented as follows.

$$aM^{2+} + (b+c) HL_{(o)} \longrightarrow M_aL_b(HL)_{C(o)} + bH^+$$
..... (1)

Where HL is the 4-acylbispyrazolone

$$K_{ex1} = \frac{[M_a L_b (HL)_C]_{(o)} [H^+]^{(b)}}{[M^{2+}]^a [HL]_{(o)}^{(b+c)}} \dots (2)$$

Where K_{ex1} is the extraction constant. Hence the distribution ratio D is given by:

$$\log D_1 = \log K_{ex1} + (a - 1) \log[M^{2^+}] + (b + c)$$

$$\log[HL]_o - (b) \log[H^+] \dots (3)$$

In the presence of a solvating agent such as butanol (BuOH), the distribution ration becomes:

 $\begin{array}{l} log \ D_2 = \ log K_{ex2} + (a \ - \ 1) \ log [M^{2+}] + (b \ + \ c) \ log \\ [HL]_{(o)} + d \ log \ [BuOH]_{(o)} - (b) \ log [H^+] \ \dots \dots \dots (4) \end{array}$

Where $M_a L_b(HL)_{c(o)}$ and $M_a L_b(HL)_c(BuOH)_{d(o)}$ represents the extractable metal complexes in the absence and presence of butanol respectively.

Determination of the values of a, b, c, and d for interactions between the ligand and one mole of metal in the equations can be done through evaluation of the partial derivatives of the equations by the method of slope analysis as follows:

$$\frac{d [\log D]}{d [\log [H^+]} = b$$
(5)

$$\frac{d [\log D]}{d [\log [HL]]_0} = b + c \quad (6)$$

$$\frac{d [\log D]}{d [\log [BuOH]_{(0)}]} = d$$
(7)

$$\frac{d \left[\log D \right]}{d \left[\log \left[M^{2^+} \right] \right]} = a - 1 \qquad (8)$$

If an acid is involved as a solvating agent in the extraction of the metal, the expected ion pair complex that would be extracted can be described by the following equation as proposed by previous authors [1 & 23].

$$aM^{2^{+}} + (b+c)H_{2}L_{(o)} + eHA_{(o)} \longrightarrow (H^{+})_{c}M_{a}L_{b}(HL)_{c(o)}.xA_{(o)} + (b)H^{+}.....(9)$$

$$K_{ex3} = \frac{[(H^{+})_{e}M_{a}L_{b}(HL)_{c(o)}.xA_{(o)}]_{(o)}(H^{+})^{(b)}}{[M^{2^{+}}]^{a}[H_{2}L]_{(o)}^{brc}[HA]^{c}} \dots (10)$$

 $log D_3 = logK_{ex3} + (a-1)log[M^{2+}] + (b+c)log[H_2L]_{(o)} +$ $elog[HA] + (b) logH^+ \dots(11)$

Determination of the value of e in the equations can be done through evaluation of the partial derivative of the equation by the method of slope analysis as follows:

$$\frac{d[\log D_3]}{d[\log[HA]]} = e$$
.....(12)

3.2 Effect of Some Mineral Acids on the Extraction Cr(VI)

The effect of some mineral acids (HCl, H₂SO₄, and HNO₃) on the extraction of the metal ion was studied at various acid concentrations, using the ligands (H₂Adp and H₂SP) in chloroform. This has been presented as % extraction versus acid concentration (M) in Figs. 1 and 2 and as log D versus log species concentration in Figs. 3-8.

3.3 Effect of Acids on the Metal Ion Extraction in the Presence and Absence of BuOH

The effect of the three mineral acids HCl, H_2SO_4 , and HNO_3 on the extraction of Cr(VI) in the presence and absence of BuOH as a synergist is presented in Figs. 1 and 2 for both ligands H₂Adp and H₂SP respectively. Fig 1 represents plots of % extraction of Cr(VI) against acid concentrations (M) using H₂Adp in chloroform. Results from the plots show that the extraction of Cr(VI) tends to be on the increase with increase in acid concentration. For HCl solutions, the % extraction increased from 32% (at 0.001M) to 62% (at 0.5M) into chloroform solution of the ligand H_2Adp . In the case of HNO₃, a much more remarkable increase in % extraction was observed even in the absence of a synergist. The extraction was observed to change remarkably from less than 1% at 0.001M HNO₃ acid to 82% extraction at 3M HNO₃ acid concentration. A similar profile was observed with the metal extraction (Cr(VI)) from H_2SO_4 concentrations. In this case the extraction increased slightly from 52% at 0.001M and to 66% at 1M H₂SO₄ concentrations.

Generally, optimal % extractions of 62%, 65% and 82% were observed at acid concentrations of 0.5M, 1.0M and 3.0M for HCl, H_2SO_4 and HNO₃ respectively for the extraction of Cr(VI) in the absence of BuOH into 0.01M H_2Adp in chloroform. This suggests that extraction of Cr(VI) is best favored in HNO₃ acid concentration of 3.0M using the ligand H_2Adp in chloroform.

In the presence of BuOH, synergism was observed in the extraction of Cr(VI) from solutions of all the three acids as presented in Fig. 1.Unlike extraction in the absence of BuOH, optimal % extraction of 90% was recorded at 5.0M acid

concentrations for both HNO₃ and H_2SO_4 solutions whereas for HCl solutions optimal % extraction was at 1.0M acid concentration. Furthermore, BuOH synergism was more pronounced for the extraction of Cr(VI) from HNO₃ solutions than for the other acids because at 0.001M concentrations of the acid, the % extraction increased from less than 1% to 76% extraction.



Fig 1: Variation of % Extraction of Cr(VI) with acid concentrations for H_2Adp .

Plots of Cr(VI) against acid concentrations (M) using H₂SP in chloroform in the presence and absence of BuOH is presented in Fig. 2. Results from the plot shows a similar extraction pattern in which the % extraction of Cr(VI) was increasing with increase in acid concentration. It also shows that the extraction of Cr(VI) was enhanced by the presence of BuOH as synergist in the organic phase with the exception of HNO₃ concentrations. In this case, however, it is the extraction from HCl solution that shows a remarkable increase from less than 2% extraction at 0.001M HCl concentration to 50% at 0.5M HCl concentration. This is contrast to extractions of same metal (Cr(VI) into H₂Adp in chloroform in which the synergistic effect was more pronounced for HNO₃ HCl. However, overall extraction using 0.01M H₂SP/Chloroform was best in HNO₃ solutions similar to extractions using 0.01M H₂Adp/Chloroform ligand.

Optimal % extraction of 50%, 70% and 90% at 0.5M, 2.0M and 5.0M acid concentrations were recorded for HCl, H_2SO_4 and HNO₃ respectively, for extraction of Cr(VI) into H_2SP in chloroform in the absence of BuOH. There is a striking similarity in the effect of BuOH on both ligands in the extraction of Cr (VI). For H_2SO_4 concentrations of 0.01M to 0.5M, the addition of BuOH was found to have enhanced the % extraction from 50% to 81%. A sharp drop to 64% was observed at 2.0M H_2SO_4 concentration, thereafter the drop continues gradually to 12% extraction of Cr (VI) recorded at 5.0M H_2SO_4 concentration.

Hence, BuOH synergism was more pronounced for extraction of Cr (VI) from HNO₃ and HCl solutions into organic solutions of H₂Adp and H₂SP respectively. Also, Optimum extraction was better in HNO₃ followed by H₂SO₄ and least in HCl acidic medium for extraction of Cr(VI) into organic solutions of H₂Adp and H₂SP in chloroform.



Fig 2: Variation of % Extraction of Cr(VI) with Acid Concentration for H_2SP

3.3 Mechanism of Extraction of Cr (VI)

Figure 3 shows the extraction of Cr (VI) as a plot of log D versus log [Acid]. Within the range of acid studied, slopes of zero was obtained for all the three acids (HCl, H_2SO_4 and HNO₃) which is an indication of the non-involvement of the acid as an ion pair or adduct complex species in the extraction process. Similar results have been obtained for the extraction of Mo(VI) http://www.sciencepub.net/nature

from same acids into organic solutions of H_2Adp and H_2SP [14].

Figure 4 presents a plot of log D against log [Cr] for the three acid conditions for which a slope of zero was obtained. Substituting this value into equation 8 above and solving, we obtain a solution of 1 (one). This is an indication of the involvement of 1 mole of Cr(VI) in the extraction process because log D is independent of the metal ion concentration. That shows that adduct complex species were not formed, hence c = o in equation (1).

Figure 5 shows the plot of log D versus log $[H_2Adp]$ for Cr(VI) for the three acids studied. The result gave slopes approximately equal to 1 for extractions from H_2SO_4 and HNO₃ acid solutions.

From equation (6), b + c = 1since c = o that implies that: b = 1

This is therefore an indication of the involvement of 1 mole of ligand in the extraction process. The extraction process based on CrO_2^{2+} species can be written as:

$$CrO_2^{2+} + H_2L_{(o)} \longrightarrow CrO_2(L)_{(o)} + 2H^+ \dots (13)$$

 $logD_1 = log K_{ex} + log[CrO_2^{2^+}] + log[H_2L] + pH.....(14)$ (pH \approx 0) where L = Adp

The values of log K_{ex} were found to be 4.50 and 4.90 as presented in Table 1.



Figure 3: Plot of log D Vs log [Acid] for Cr(VI) with $\rm H_2Adp$



Figure 4: Plots of log D Vs log [Cr] with H₂Adp



Figure 5: Plot of log D Vs log $[H_2Adp]$ for Cr(VI) with H_2Adp .

However, in figures 6, 7 and 8 involving the H_2SP ligand, figure 6 recorded a slope of 1, an indication that there may be an ion pair complex species involving HCl. Solving equation (12) gives a value of e = 1.

Figure 7 simply shows that log D is independent of log [Cr] which is taken as an indication

of the involvement of 1 mole of chromium in the extraction process. Thus if that is the case that means that the Cr (VI) species involved in the extraction process is definitely not the CrO_2^{2+} species used in equation (14). Figure 8 also recorded a slope of 1 indicating that 1 mole of the H₂SP ligand is involved in the extraction of chromium, when solved following the sequence of argument presented above. Therefore, the extraction of Cr(VI) involving this ligand in the presence of these acids can be written first as an acidification process [24 - 25] followed by the extraction of species as ion pair complexes as shown: $CrO_4^{2-} + H^+ \xrightarrow{I} HCrO_4^{-} \dots \dots (15)$ $HCrO_4 - H_2SP_{(0)} + H^+ \xrightarrow{I} H_4CrO_4^{2+}SP^{2-}_{(0)}$ (16) [H₄CrO₄²⁺SP²⁻]₍₀₎ (17) Kex $[HCrO_4^{-}] [H_2SP]_{(0)} [H^+]$

$$log K_{ex} = log D + log [H_2SP] - log [H^+] (18)log D = log K_{ex} + log [H_2SP] + log [H^+] (19)$$

The calculated log K_{ex} was found to be 4.70 and is presented in Table 1. Evidence of the acidification process involving CrO_4^{2-} ion has been previously reported [24 - 25].

Thus the extracted complexes are shown in table 1.0 below.



Fig 6: Plot of log D Vs log [HCl] for Cr(VI) in H₂SP



Fig 7: Plot of log D Vs log [Cr] in H₂SP



Fig 8: Plot of log D Vs log [H₂SP] for Cr(VI)

Table 1: Data on extraction of the metals with H_2Adp and H_2SP at room temperature.

Metal	Acid	Ligand	log	Extracted
			Kex	Specie
Cr(VI)	H_2SO_4	H ₂ Adp	4.90	CrO ₂ (Adp)
	HNO ₃	H ₂ Adp	4.52	CrO ₂ (Adp)
Cr(VI)	HC1	H_2SP	4.70	$H_4CrO_4^{2+}(SP)^{2-}$

4.0 Conclusion

Liquid – liquid extraction of chromium (VI) ions from concentrations of various mineral acids (HCl, H_2SO_4 and HNO₃) using chloroform solution of the ligand 4-adipoylbis(1-phenyl-3-methylpyrazolone-5), H_2Adp in the absence of butanol (BuOH) gave optimal % extraction of 62%, at 0.5M acid concentration for HCl and 66% at 1.0M for H_2SO_4 . While 82% at 3.0M acid concentration was equally obtained for HNO₃. Extractions using chloroform solution of 4sebacoylbis(1-phenyl-3-methylpyrazolone-5), H_2SP in the absence of butanol (BuOH) gave optimal % extraction of 50%, 70% and 90% at 0.5M, 2.0M and 5.0M acid concentrations for HCl, H_2SO_4 and HNO₃ respectively, for the extraction of Cr(VI).

In the presence of BuOH, synergism was more pronounced for extraction of Cr (VI) from HNO₃ and HCl solutions into chloroform solutions of H₂Adp and H₂SP respectively. However, optimum extraction was better in HNO₃ media followed by H₂SO₄ and least in HCl acidic media for extraction of Cr(VI) into organic solutions of 0.01M H₂Adp/chloroform and 0.01M H₂SP/chloroform in both the absence and presence of BuOH.

Mechanism of the extraction systems showed that extraction using the ligand H₂SP/chloroform involved only one(1) mole of the ligand. Also, the interaction first involved an acidification process followed by the extraction species as ion pair complexes and thus its extracted specie was $H_4CrO_4^{2+}(SP)^{2-}$. This behavior was however not observed for extraction using the ligand H₂Adp/chloroform, here, the interaction involved two(2) moles of the ligand and does not involve acidification first. Hence, its extracted specie was $CrO_2(Adp)$. Finally, the calculated average log K_{ex} value was 4.70.

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